

PISTACHIOSHELL CARBON AS A NADSORBENTA COMPARATIVE STUDY ON ADSORPTION OF MONOBASIC AND DIBASIC ACID

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Abstract

In this study, adsorption of different monobasic and dibasic acids was performed on pistachio shell carbon, which was used as an adsorbent, as it serves as eco-friendly adsorbents. It has proven to be significantly effective with the provision of satisfactory adsorption capacities for the removal of pollutants from waste water. We have studied adsorption on different monobasic and dibasic acid by taking pistachio shell carbon as an adsorbent.

The monobasic acids and dibasic acids under study were Acetic acid, Propionic acid, oxalic acid and Succinic acid. Pistachio nut shell is the best material that can be made into carbon as they have a lot of micropores, low ash content high water Solubility and high reactivity. Pistachio nut shell carbon has become one of the best forms of carbon for water filtration and water Purification in recent years. Additionally, it can effectively absorb certain impurities.

Pistachio nut shell carbon referred to a wide range of carbonaceous materials with a high degree of porosity and an extended inter particulate surface area and widely used adsorbent in waste water treatment throughout the world.

In the very first step we collect pistachio nut shell and remove dirt and unwanted substances from it. Then the shell is smashed and crushed and put it in a container or furnace and get it for heating. The heating is done until the pistachio nut shell by product it is the pistachio nut shell processed into carbonation of the latter to produce pistachio nut shell carbon in the form of burned carbon. In the run of burning of pistachio nut shell, the heating temperature should be programmed to increase from the room temperature to the desired carbonization temperature. The overall preparation is by chemical method.

Pistachio nut shell carbon is frequently used in everyday life, industry food production, medicine, pharmacy etc. and is used for adsorption of organic substances and non-polar adsorbate and it is also usually used for waste gas and waste water treatment. It is the most widely used adsorbent since most of its chemical (example surface groups) and physical properties (example pore size distribution and surface area) can be turned according to what is needed. Its usefulness also derives from its large micropore (and sometimes meso-pores) volume and the resulting high surface area.

The adsorption isotherm for Langmuir adsorption isotherm and Freundlich adsorption isotherm was studied for different monobasic and dibasic acid by taking pistachio shell carbon as an adsorbent.

The results obtained when compared with different acids the conclusion obtained was compared with different monobasic acids (Acetic acid and Propionic acid) dibasic acids (oxalic acid, succinic

acid). From the readings obtained we observed that extent of adsorption of propanoic acid is greater than acetic acid. i.e. propanoic acid (0.01221) > acetic acid (0.01166)

the reason behind the above conclusion is the presence of CH_2 group in propanoic acid and absence of CH_2 group in acetic acid. the extent of adsorption of succinic acid is greater than oxalic acid.

i.e., succinic acid (0.01263) > oxalic acid (0.01182)

the reason behind the above conclusion is the presence of 2CH_2 group in succinic acid or absence of 2CH_2 group in oxalic acid.

Introduction:

Adsorption is the adhesion of atoms, ions or molecules from a gas liquid or dissolved solid to a surface. This process creates a film of the adsorbate on the surface of the adsorbent. Adsorption is present in many natural, physical, biological and chemical system and is widely used in industrial applications such as heterogeneous catalysts, Coconut shell Carbon, capturing and using waste heat to provide cold water for air conditioning and other process requirements. Garlic processing by-products include skins, outer leaves, tops, and bottoms. Currently, these materials are disposed of in landfills or used as soil amendments, which result in negative environmental impacts and phytotoxicity to plants, respectively. These materials need to be economically and environmentally managed.

Natural adsorbents are plentiful, inexpensive, require little processing, and are effective in removing pollutants. Natural adsorbents are divided into four groups based on their availability status: waste materials from agricultural, fruit waste, plant waste, and bio adsorbents. Solids agricultural wastes are a cheap and abundant source of resources. Sugarcane bagasse, rice husk, oil palm shell, cotton waste, cashew nutshell, garlic peel, almond shell, and other agricultural waste adsorbents can be used to remove pollutants effectively.

Grapefruit peel, orange peel, mosambi peel, mandarin peel, banana peel, raw date pits, jack fruit peel, pomegranate peel, muskmelon peel, and palm fruit bunch are examples of fruit waste that can be utilized as adsorbents. Plant waste such as plant leaf powder, tea waste, wood chips, saw dust, plant fibre, wood shavings, jute stick powder, oil palm wood, bark, neem leaf powder, and pine sawdust, can all be employed as adsorbents to eliminate pollutants from aqueous solutions. Hair, yeast, chitin and fungi, chitosan, biomass, peat, and eggshell are examples of bio adsorbents that can be utilized for adsorption.

Pistachio processing by-products include pistachio shell. Currently, these materials are disposed of in land or used as soil amendments, which result in negative environmental impacts and phytotoxicity to plants, respectively. These materials need to be economically and environmentally managed.

For the aim of wastewater treatment, the biosorption of Cr(VI) by the pistachio nut shell in a batch-type reactor was researched in depth. To maximize Cr(VI) removal from aqueous solutions and equilibrium isotherms and kinetic data, the effects of initial Cr(VI) concentration, time, and pH were explored. From a solution containing 3000 ppm of Cr, the pistachio nut shell adsorption capacity was reported to be 103.09 mg/g of

adsorbent (VI). It can be concluded that the Langmuir adsorption isotherm was more appropriate for explaining equilibrium than the Freundlich adsorption isotherm. Gibbs' free energy was spontaneous for all interactions, and the adsorption process had exothermic enthalpy values.

The effects of various experimental conditions on the removal of Cu ions from aqueous solution by pistachio nut shell were investigated. The point of zero charges for pistachio nut shell was between 4.55 to 4.75. The adsorption capacity of the pistachio nut shell was found to be 66.7 mg/g at pH 5.3 and T = 303 K.) The pseudo-second-order kinetic model fitted the batch data adequately. The rate constant of pistachio scale in the absence of diffusional resistance was estimated to be 0.075 mg/g/min respectively at 303 K. The thermodynamic studies showed that the Cu ions adsorption on the pistachio skin was spontaneous and endothermic.

Water contamination by fluoride is a major concern in many places of the world. When its concentration in drinking water is more than 1.5 mg/L, which is the maximum allowable concentration of fluoride by the World Health Organization (WHO), it can become harmful to people's health, for example, causing dental or skeletal fluorosis.

So, it is quite urgent to develop more advanced and cost-effective techniques to decrease and remove fluoride from the water. Several defluoridation technologies of drinking water, such as ion exchange, precipitation-coagulation, reverse osmosis, electrodialysis and nano filtration, have been developed for fluoride removal from water.

The cheapest and effective way to overcome from these problem is adsorption by bio waste, for example pistachio nut shell carbon. Pistachio nut shell carbon as an adsorbent, as we know that adsorbents play a very vital role in the adsorption processes. Pistachio nut shell is low cost adsorbent, we have simply used the criteria of low cost as well as eco-friendly adsorbents. It has proven to be significantly effective with the provision of studied adsorption on different monobasic and dibasic acid by taking pistachio nut shell carbon as an adsorbent.

ISOTHERMS

The adsorption of gases and solutes is usually described through isotherms, i.e. the amount of adsorbate on the adsorbent as a function of its pressure (if gas) or concentration (for liquid phase solutes) at constant temperature. The quantity adsorbed is nearly always normalized by the mass of the adsorbent to allow comparison of different materials. To date, 15 different isotherms models have been developed.

FREUNDLICH ADSORPTION ISOTHERM

The first mathematical fit to an isotherm was published by Freundlich and Kuster (1906) and is purely empirical formula for gaseous adsorbates:

$$x/m = Kp^{1/n}$$

Where X is the mass of adsorbate adsorbed, m is the mass of the adsorbent, p is the pressure of adsorbate (this can be changed to concentration if investigation solution rather than gas), and k and n are the empirical constant for each adsorbent- adsorbate pair at a given temperature.

LANGMUIR ADSORPTION ISOTHERM

Irving Langmuir was the first to devise a scientifically based adsorption isotherm in 1918. The model applies to gases adsorbed on solid surfaces. It is a semi-empirical isotherm with a kind basis and was derived based on statistical thermodynamics.

If we define surface coverage, θ as the fraction of the adsorption sites occupied, in the equilibrium we have:

$$K = k/k_{-1} = \theta / (1 - \theta)P,$$

Or

$$\theta = KP / 1 + KP,$$

Where P is the partial pressure of the gas or the molar concentration of the solution. For every low pressure $\theta \approx KP$, and for high pressure $\theta \approx 1$.

ADSORBENT USED



Fig.1 pistachio nut shell



Fig.2 crushed pistachio Nut shell



Fig.3 pistachio nut shell carbon

The use of pistachio nut shell carbon as an adsorbent of the industrial pollutant is a new trend. The pistachio nut shell carbon has a capability as an adsorbent since it has high carbon content and density low ash content and uniform pore distribution. As an agriculture waste material, the use of pistachio nut shell carbon also becomes a solution for environment. Problems with a low-cost production. Moreover, Iran is a tropical country that provides a large number of pistachio nut shell as a raw material for carbon.

Pistachio nut shell carbon referred to a wide range of carbonaceous materials with a high degree of porosity and an extended inter particulate surface area and widely used adsorbent in waste water treatment throughout the world.

Pistachio nut shell carbon are unique and versatile adsorbent and they are used for the removal of undesirable odour, colour, taste, and other organic and inorganic impurities (generally referred to as adsorbates) from domestic and industrial wastes, for air purification in inhabited places, restaurants, food processing, removal of color from various syrups and pharmaceutical products, in air pollution control from industrial and automobile exhaust and in a variety of gas phase applications. They are also well known for

their applications in medicine for the removal of toxins and bacterial infections in certain alignments.

Adsorption by pistachio nut shell carbon is one of the most frequently used method to remove organic compounds from water, because pistachio nut shell carbon possess perfect adsorption ability for chloro phenols. In this project, the objective is to investigate how the adsorption capacity of pistachio nut shell carbon is influenced by elevated temperature using different concentrations of para-chlorophenol as the adsorbate.

STRUCTURE OF PISTACHIO NUT SHELL CARBON

Adsorption takes place at the surface of pistachio nut shell carbon. The surface characteristics of pistachio nut shell carbon play a crucial role in adsorption from aqueous solutions and catalytic properties of carbon. The structure of pistachio nut shell carbon is classified based on the activities that occur at the surface of the carbon. The structure of pistachio nut shell carbon surface can therefore be viewed in two dimensions namely, physical structure and chemical structure.

PHYSICAL STRUCTURE OF PISTACHIO NUT SHELL CARBON

This refers to how the atoms of pistachio nut shell carbon is linked together and how this arrangement actually give rise to the adsorption ability of pistachio nut shell carbon it also describes the various for sizes available on the surface of pistachio nut shell carbon which is responsible for its wide range of applicability in the sense that the four size of any particular pistachio nut shell carbon determine to a large extent what it is used for. The physical structure of pistachio nut shell carbon is further divided into:

POROUS STRUCTURE

Non-graphitizing carbon (i.e. pistachio nut shell carbon with a random arrangement of microcrystalline, strong cross-linking between neighbouring crystallites and well-developed porous structure) was found to have relatively low density (less than 2 gm/cm^3). The porous structure formed during carbonization process is further developed during activation process.

Activation process is a process through which small, low volume pores which increase the surface area of carbon are created within its structure by either heating carbon at temperature changes between 600 to 1200 degree celsius in the absence of oxygen or by impregnating carbon with certain chemicals such as acids, strong bases or salt followed by heating at low temperatures of about 400 to 700 degree Celsius. This process enlarges the diameter of the pores and improve their volume. The nature of the raw material used for the carbonization determines the structure of the pores generated and the pore size distribution. Activation carbon pores are categorized based on their size and their function. Based on their function, we have,

particles consisting of gaps between carbon plates of about 1-5 molecular diameter in size.

PORES FOR TRANSPORT: these are the largest pores within the particle. They vary from pores greater than 5 molecular diameter to visible cracks. They consist of a variety of different sizes and shapes.

Based on their sizes, 3 groups of pores can be distinguished and they are:

- Micro-pores (<2 nm diameter)
- Meso-pores (2-50 nm diameter)
- Macro-pores (>50 nm diameter)

Micro-pores generally contribute to the bulk part of the internal surface area while meso-pores are generally regarded as highways into the carbon particles and are crucial kinetics. According to Dunin and Zaverina, a micro-porous active carbon is produced when the degree of burn-off is less than 50%, micro-porous active carbon is produced when the extent of burn-off is between 50% and 75%, the product will contain a mixture of all types of pores.

The classification of pores by the Dunin is based on their width which represents the distance between the walls of a slit shaped pore. This classification has now been adopted by the international union for pure and applied chemistry.

Adsorption in micropores whose effective radius is less than 2 nm occurs through volume filling with no capillary condensation taking place. The adsorption energy in micro-pores is much larger compared to other pore types, their volume range between 0.15-0.70 cm³/gm.

PREPARATION OF PISTACHIO NUTSHELL CARBON

In the very first step we collect pistachio nut shell and remove dirt and unwanted substances from it. Then the shell is smashed and crushed and put it in a container or furnace and get it for heating. The heating is done until the pistachio nut shell by product it is the pistachio nut shell processed into carbonation of the latter to produce pistachio nut shell carbon in the form of burned carbon. In the run of burning of pistachio nut shell, the heating temperature should be programmed to increase from the room temperature to the desired carbonization temperature. The overall preparation is by chemical method.

Adsorption process by different mono basic acid (Acetic acid, Propionic acid) dibasic acid (Oxalic acid and Succinic acid)

Materials Used: pistachio nut shell carbon, Mono basic acid (Acetic acid and Propionic acid) Dibasic acids (Oxalic acid and Succinic acid), NaOH, Phenolphthalein, Stopped bottle, Burette, Pipette, Funnel, Conical flask.

PROCEDURE:

Prepared aqueous solution of acids into numbered flask as labelled, the total volume of each solution is 50 ml taken in Stopped bottles. Transfer 10 ml of the solution from each bottle into the conical flask. Add 2-3 drops of Phenolphthalein indicator and titrate against NaOH. Once the end point is reached, read the burette reading. The volume of base V_1 . Calculate the actual concentration of oxalic acid C_1 in the flask number 1 to 5 respectively, and write it down in the table. Using practical balance weigh 5 portions of pistachio nut shell carbon, each portion 1 gram. Put pistachio nut shell carbon into numbered flask into stoppers and shake them, wait for 20 minutes, the process of adsorption is in progress. Mix the mixtures for

several times by shaking the flask. (The process of adsorption is a function of times it is important to put onion peel into flask at the same time to provide adsorption for the same period in each flask). Filter the mixtures into clean and dry flask to avoid disturbing effect of adsorption of acid into filtering paper, remove away the first portion of filtration approximate of 5ml. Determine the final concentration of acid C, in each of the flask after adsorption from each solution, pipette out 10ml of oxalic acid solution and transfer it to clean and dry conical flask. To this conical flask containing oxalic acid solution at 2 to 3 drops of Phenolphthalein indicator. Now, titrate this solution against NaOH in the burette, note down the burette reading. The volume of base V_2

PROCEDURE TABULAR COLUMN:

Dilution of acid

Bottle No.	Vol. of acid added (0.5N)	Volume of water added in ml	Amount of pistachio nut shell carbon added in gm
1	50	00	1
2	40	10	1
3	30	20	1
4	20	30	1
5	10	40	1

TABULAR COLUMN: Acetic acid

INO.	Initial concentration of acetic acid (C_0)	Vol. of titrant taken in ml	Amt. of pistachio shell carbon added in gm	Burette reading	$C_e = B.R \times 0.1 / 10$ Eq. conc. of acid in mol/dm ³	$X = C_0 - C_e / 20$ amount adsorbed in moles	x/m	$\log(x/m)$	$\log C_e$	$C_e(x/m)$
1	0.5	10	1	10.8	0.108	0.0196	0.0196	-1.70774	-0.9665	0.002168
2	0.4	10	1	8.9	0.089	0.01555	0.01555	-1.8082	-1.050	0.0013839

								6	6	
3	0.3	10	1	6.7	0.067	0.01165	0.01165	-1.93367	-1.1739	0.0007805
4	0.2	10	1	4.7	0.047	0.00765	0.00765	-2.11633	-1.3279	0.0003595
5	0.1	10	1	2.3	0.023	0.00385	0.00385	-2.41453	-1.6382	0.0000885

TABULAR COLUMN: Propionic acid

SINO.	Initial concentration of propionic acid	Vol. of titrant taken in ml	Amt. of propionic acid added in ml	Burette reading	$C_e = B \cdot R \times 0.1 / 10$ Eq. conc. of acid in moles	$X = C_0 - C_e$ 20 amount adsorbed in moles	x/m	$\text{Log}(x/m)$	$\text{Log } C_e$	$C_e(x/m)$
1	0.5	10	1	9.5	0.095	0.02025	0.02025	-1.69357	-1.02227	0.00192375
2	0.4	10	1	7.7	0.077	0.01615	0.01615	-1.79182	-1.11350	0.00124355
3	0.3	10	1	5.5	0.055	0.01225	0.01225	-1.91186	-1.25963	0.00067375
4	0.2	10	1	3.3	0.033	0.00835	0.00835	-2.07831	-1.48148	0.00027555
5	0.1	10	1	1.9	0.019	0.00405	0.00405	-2.39254	-1.72124	0.00007695

TABULAR COLUMN: Oxalic acid

SINO.	Initial concentration of oxalic acid (C_0)	Vol. of titrant taken in ml	Amt. of potassium dichromate added in ml	Burette reading	$C_e = B.R \times 0.1 / 10$ Eq. conc. of acid in mol/dm ³	$X = C_0 - C_e / 20$ amount adsorbed in moles	x/m	$\log(x/m)$	$\log C_e$	$C_e(x/m)$
1	0.5	10	1	10.4	0.104	0.0198	0.0198	-1.7033	-0.9829	0.0020592
2	0.4	10	1	8.6	0.086	0.0157	0.0157	-1.8041	-1.0655	0.0013502
3	0.3	10	1	6.2	0.062	0.0119	0.0119	-1.9244	-1.2076	0.0007378
4	0.2	10	1	4.4	0.044	0.0078	0.0078	-2.1079	-1.3565	0.0003432
5	0.1	10	1	2.2	0.022	0.0039	0.0039	-2.4089	-1.6575	0.0000858

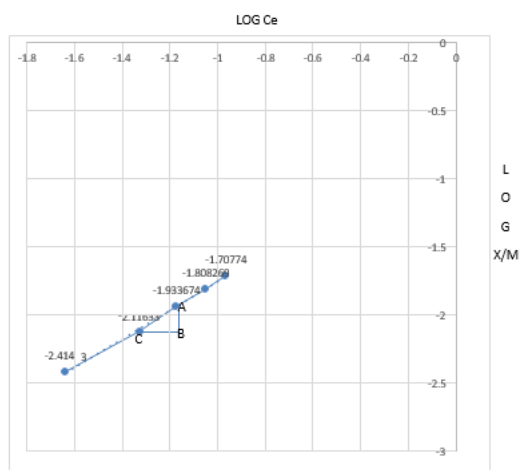
TABULAR COLUMN: Succinic acid

SINO.	Initial concentration of succinic acid (C_0)	Vol. of titrant taken in ml	Amt. of potassium dichromate added in ml	Burette reading	$C_e = B.R \times 0.1 / 10$ Eq. conc. of acid in mol/dm ³	$X = C_0 - C_e / 20$ amount adsorbed in moles	x/m	$\log(x/m)$	$\log C_e$	$C_e(x/m)$
1	0.5	10	1	7.8	0.078	0.0211	0.0211	-1.6757	-1.1079	0.0016458

								1		
2	0.4	10	1	6.4	0.064	0.0168	0.0168	-1.77469	-1.1938252	0.00107
3	0.3	10	1	4.4	0.044	0.0128	0.0128	-1.89279	-1.3565432	0.00056
4	0.2	10	1	3.4	0.034	0.0083	0.0083	-2.08092	-1.4685222	0.00028
5	0.1	10	1	1.7	0.017	0.00415	0.00415	-2.38195	-1.76955055	0.00007

Graphs

GRAPH: FREUNDLICH ADSORPTION ISOTHERM (ACETIC ACID)



Scale= X-axis- 1 unit =0.5cm

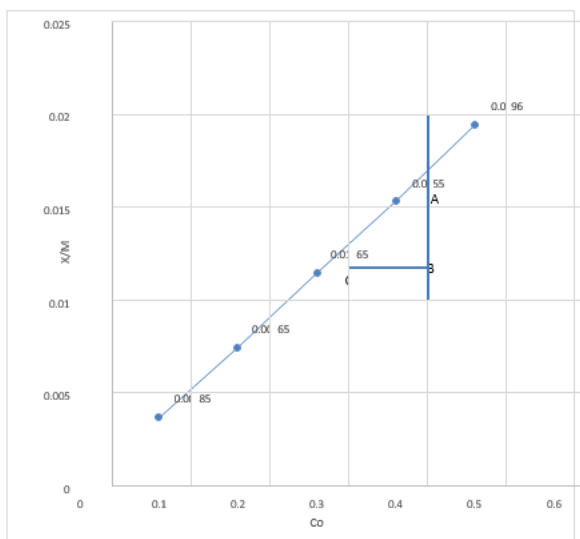
Y-axis- 1 unit=0.5cm

SLOPE= $\frac{AB}{BC}$

$$= \frac{(-1.933674) - (-1.163)}{(-1.17) - (-1.32)}$$

$$= \frac{0.182656}{0.15}$$

$$= 1.217$$

GRAPH : LANGMUIR ADSORPTION ISOTHERM (ACETIC ACID)

Scale= X-axis- 1 unit =0.1cm

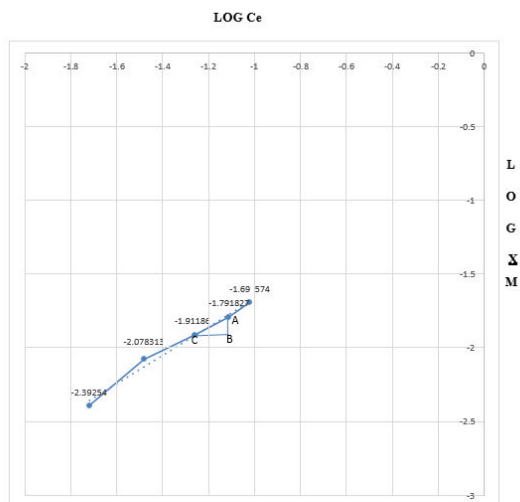
Y-axis- 1 unit=0.005cm

SLOPE= $\frac{AB}{BC}$

$$= \frac{0.0155-0.01165}{0.4-0.3}$$

$$= \frac{0.00385}{0.1}$$

$$= 0.0385$$

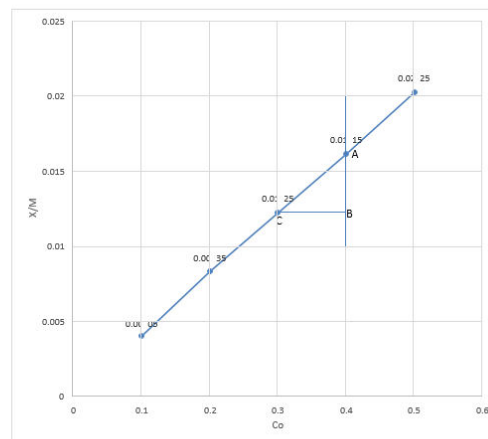
GRAPH: FREUNDLICH ADSORPTION ISOTHERM (PROPANOIC ACID)

Scale= X-axis- 1 unit =0.5cm

Y-axis- 1 unit=0.5cm

SLOPE= $\frac{AB}{BC}$

$$= \frac{(-1.79182)-(-1.91186)}{(-1.11)-(-1.25)}$$

GRAPH : LANGMUIR ADSORPTION ISOTHERM (PROPANOIC ACID)

Scale= X-axis- 1 unit =0.1cm

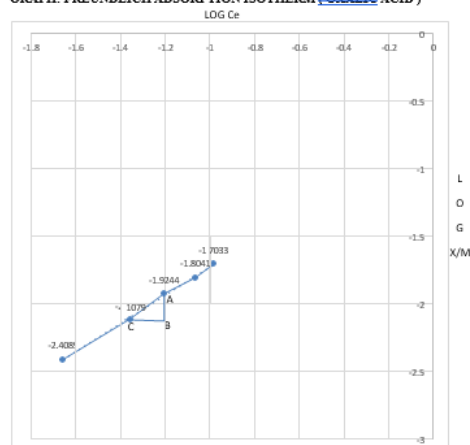
Y-axis- 1 unit=0.005cm

SLOPE= $\frac{AB}{BC}$

$$= \frac{0.01615-0.01225}{0.4-0.3}$$

$$= \frac{0.0039}{0.1}$$

GRAPH: FREUNDLICH ADSORPTION ISOTHERM (OXALIC ACID)

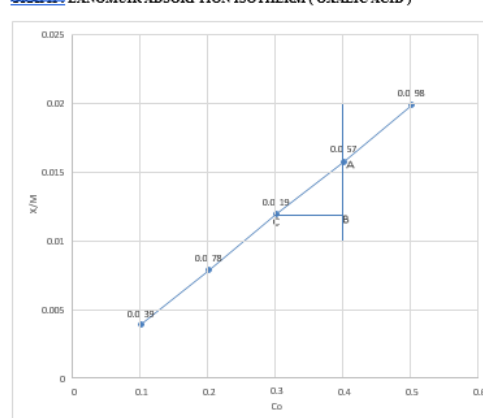


Scale= X-axis- 1 unit =0.5cm

Y-axis- 1 unit=0.5cm

$$\begin{aligned} \text{SLOPE} &= \frac{AB}{BC} \\ &= \frac{(-1.8244) - (-2.1079)}{(-1.20) - (-1.55)} \\ &= \frac{0.1835}{0.15} \\ &= 1.22 \end{aligned}$$

GRAPH: LANGMUIR ADSORPTION ISOTHERM (OXALIC ACID)

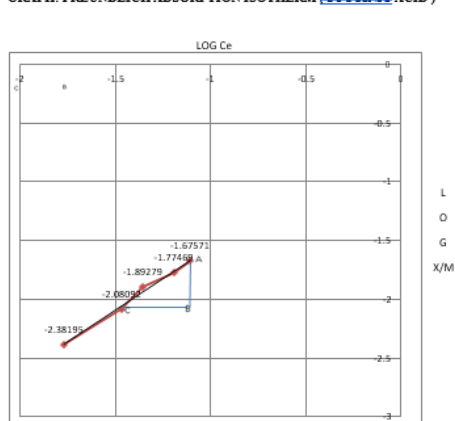


Scale= X-axis- 1 unit =0.1cm

Y-axis- 1 unit=0.005cm

$$\begin{aligned} \text{SLOPE} &= \frac{AB}{BC} \\ &= \frac{0.0157 - 0.0119}{0.4 - 0.3} \\ &= \frac{0.0038}{0.1} \\ &= 0.038 \end{aligned}$$

GRAPH: FREUNDLICH ADSORPTION ISOTHERM (SUCCINIC ACID)

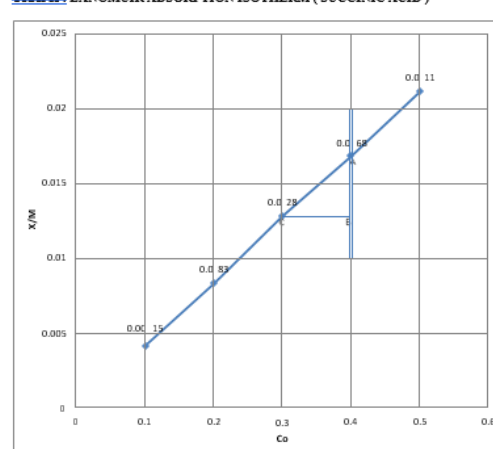


Scale= X-axis- 1 unit =0.5cm

Y-axis- 1 unit=0.5cm

$$\begin{aligned} \text{SLOPE} &= \frac{AB}{BC} \\ &= \frac{(-1.77469) - (-2.08092)}{(-1.19) - (-1.46)} \\ &= \frac{0.30623}{0.27} \\ &= 1.1341 \end{aligned}$$

GRAPH: LANGMUIR ADSORPTION ISOTHERM (SUCCINIC ACID)



Scale= X-axis- 1 unit =0.1cm

Y-axis- 1 unit=0.005cm

$$\begin{aligned} \text{SLOPE} &= \frac{AB}{BC} \\ &= \frac{0.0168 - 0.0128}{0.4 - 0.3} \\ &= \frac{0.004}{0.1} \\ &= 0.04 \end{aligned}$$

APPLICATIONS OF ADSORPTION

The phenomenon of adsorption finds extensive applications in industry, in laboratory and also in various chemical processes. A few important applications are listed below:

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1. Removal of coloring matter:

Many substances such as sugar, juice and vegetable oils are colored due to the presence of impurities. They can be decolorized by placing in contact with adsorbent like Coconut shell Carbon or fuller's earth. Similarly most of the organic compounds that are synthesized in the laboratory are colored. They can also be decolorized with the help of animal Carbon.

2. In gas masks:

Coconut shell Carbon is generally used in gas masks to adsorb poisonous and toxic gases from air. These masks are used by the miners since there is atmosphere of CO and other such gases prevailing in the coal mines.

3. In separating noble gases:

Coconut shell coconut Carbon has the capacity to adsorb the noble gases present in a mixture (except radon) at different temperatures. This helps in the separation of these gases. The process of separation has been discussed in detail in competition focus.

4. In dying of cloth:

Mordants such as alums are used in dying of cloth. The adsorbed dye particles which otherwise do not stick to the cloth.

5. In dehumidizers:

Silica Gel is commonly employed to adsorb humidity or moisture from air. This is necessary for the storage of delicate instruments which might otherwise be damaged by contact with moist air.

6. Heterogeneous catalysts:

The use of metal catalyst such as Fe, Ni, Pd, etc.. In the manufacturing process such as contact process, Haber process and the hydrogenation of oils etc is based upon the phenomenon of adsorption.

7. In chromatography:

The different chromatography techniques such as adsorption, paper or column chromatography which are used for the purification and the separation of substances available in small amounts, are based upon the theory of selective adsorption.

8. In ion exchange resins:

The organic polymers containing groups like $-\text{COOH}$, $-\text{SO}_3\text{H}$, $-\text{NH}_2$ etc possess the property of selective adsorption of ion from solution. These are quite useful in the softening of water and also in the separation of the elements of the lanthanide series (also called as rare earths) from the mixture.

9. In quantitative analysis:

Certain qualitative test such as the lake test for the confirmation of Al^{3+} ions are based upon adsorption, ie $Al(OH)_3$, has a capacity to adsorb the colour of blue litmus from the solution.

10. In adsorption indicators:

Many titrations involving precipitating reactions, dyes such as eosin and fluorescein are used as adsorption indicators. This is based upon the fact that, these are more adsorbed by the precipitates than by the solution.

11. In creating high vacuum:

In some experiments very high vacuum is needed which means that, the air from the vessels has to be completely evacuated. Vacuum pumps are used for the purpose However, Carbon can be used to remove last traces of air to achieve very high vacuum. It adsorbs the different gases present in air.

12. In froth floatation process:

In this process, commonly used for the concentration of sulphide ores containing some earthy impurities (gangue) mainly carrying silica.

CONCLUSION

Comparison of difference between monobasic acids (acetic acid and propanoic acid).

From the readings obtained we observed that extent of adsorption of propanoic acid is greater than acetic acid.

i.e. propanoic acid (0.01221) > acetic acid (0.01166)

The reason behind the above conclusion is the presence of CH_2 group in propanoic acid and absence of CH_2 group in acetic acid.

Comparison of difference between dibasic acid (oxalic acid and succinic acid)

From the readings obtained we observe that the extent of adsorption of succinic acid is greater than oxalic acid.

i.e. succinic acid (0.01263) > oxalic acid (0.01182)

The reason behind the above conclusion is the presence of $2CH_2$ group in succinic acid or absence of $2CH_2$ group in oxalic acid.

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