

EVALUATION OF PISTACHIONUT SHELLDERIVED ACTIVATED CARBONASAN ADSORBENTFOR UPTAKE OF DIFFERENTDIBASICACIDS

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Abstract

In this study, adsorption of different dibasic acids was performed on pistachio shell carbon, which was used as an adsorbent, as it serves as eco-friendly adsorbents. It has proven to be significantly effective with the provision of satisfactory adsorption capacities for the removal of pollutants from waste water. We have studied adsorption on different dibasic acid by taking pistachio shell carbon as an adsorbent.

The dibasic acids under study were oxalic acid, malonic acid, succinic acid and Glutaric acid. Pistachio nut shell is the best material that can be made into carbon as they have a lot of micropores, low ash content, high water solubility and high reactivity. Pistachio nut shell carbon has become one of the best forms of carbon for water filtration and water purification in recent years. Additionally, it can effectively absorb certain impurities.

In the very first step, we collect pistachio nut shell and remove dirt and unwanted substances from it. Then the shell is smashed and crushed and put it in a container or furnace and get it for heating. The heating is done until the pistachio nut shell by product it is the pistachio nut shell processed into carbonation of the latter to produce pistachio nut shell carbon in the form of burned carbon. In the run of burning of pistachio nut shell, the heating temperature should be programmed to increase from the room temperature to the desired carbonization temperature. The overall preparation is by chemical method.

The adsorption isotherm for Langmuir adsorption isotherm and Freundlich adsorption isotherm was studied for different dibasic acids by taking pistachio shell carbon as an adsorbent.

The results obtained when compared with different acids the conclusion obtained was compared with different dibasic acids (oxalic acid, malonic acid, succinic acid and glutaric acid). From the readings obtained it was observed that the extent of adsorption of oxalic acid (0.01182), malonic acid (0.01166), succinic acid (0.01263) and glutaric acid (0.01221). Reason behind the above conclusion may be the presence of CH_2 group. The extent of adsorption of succinic acid (0.01263) > oxalic acid (0.01182). The reason behind the above conclusion is the presence of 2CH_2 group in succinic acid or absence of 2CH_2 group in oxalic acid.

Introduction:

Adsorption is the adhesion of atoms, ions or molecules from a gas, liquid or dissolved solid to a surface. This process creates a film of the adsorbate on the surface of the adsorbent. Adsorption is present in many natural, physical, biological and chemical systems and is widely used in industrial applications such as heterogeneous catalysts, Coconut shell Carbon, capturing and using waste heat to provide cold water for air conditioning and other processes.

requirements. Garlic processing by-products include skins, outer leaves, tops, and bottoms. Currently, these materials are disposed of in landfills or used as soil amendments, which result in negative environmental impacts and phytotoxicity to plants, respectively. These materials need to be economically and environmentally managed.

Natural adsorbents are plentiful, inexpensive, require little processing, and are effective in removing pollutants. Natural adsorbents are divided into four groups based on their availability status: waste materials from agricultural, fruit waste, plant waste, and bio adsorbents. Solids agricultural wastes are a cheap and abundant source of resources. Sugarcane bagasse, rice husk, oil palm shell, cotton waste, cashew nutshell, garlic peel, almond shell, and other agricultural waste adsorbents can be used to remove pollutants effectively.

Pistachio processing by-products include pistachio shell. Currently, these materials are disposed of in landfills or used as soil amendments, which results in negative environmental impacts and phytotoxicity to plants, respectively. These materials need to be economically and environmentally managed.

For the aim of wastewater treatment, the biosorption of Cr(VI) by the pistachio nut shell in a batch-type reactor was researched in depth. To maximize Cr(VI) removal from aqueous solutions and equilibrium isotherms and kinetic data, the effects of initial Cr(VI) concentration, time, and pH were explored. From a solution containing 3000 ppm of Cr, the pistachio nut shell adsorption capacity was reported to be 103.09 mg/g of adsorbent (VI). It can be concluded that the Langmuir adsorption isotherm was more appropriate for explaining equilibrium than the Freundlich adsorption isotherm. Gibbs' free energy was spontaneous for all interactions, and the adsorption process had exothermic enthalpy values.

Water contamination by fluoride is a major concern in many places of the world. When its concentration in drinking water is more than 1.5 mg/L, which is the maximum allowable concentration of fluoride by the World Health Organization (WHO), it can become harmful to people's health, for example, causing dental or skeletal fluorosis.

Pistachio nut shell carbon as an adsorbent, as we know that adsorbents play a very vital role in the adsorption processes. We have simply used the criteria of eco-friendly adsorbents. It has proven to be significantly effective with the provision of studied adsorption on different monobasic and dibasic acid by taking pistachio nut shell carbon as an adsorbent.

ISOTHERMS

The adsorption of gases and solutes is usually described through isotherms, i.e. the amount of adsorbate on the adsorbent as a function of its pressure (if gas) or concentration (for liquid phase solutes) at constant temperature. The quantity adsorbed is nearly always normalized by the mass of the adsorbent to allow comparison of different materials. To date, 15 different isotherms models have been developed.

FREUNDLICH ADSORPTION ISOTHERM

The first mathematical fit to an isotherm was published by Freundlich and Kuster (1906) and is purely empirical formula for gaseous adsorbates:

$$x/m = Kp^{1/n}$$

Where X is the mass of adsorbate adsorbed, m is the mass of the adsorbent, p is the pressure of adsorbate (this can be changed to concentration if investigation solution rather than gas), and k and n are the empirical constant for each adsorbent- adsorbate pair at a given temperature.

LANGMUIR ADSORPTION ISOTHERM

Irving Langmuir was the first to devise a scientifically based adsorption isotherm in 1918. The model applies to gases adsorbed on solid surfaces. It is a semi-empirical isotherm with a kind basis and was derived based on statistical thermodynamics.

If we define surface coverage, θ as the fraction of the adsorption sites occupied, in the equilibrium we have:

$$K = k/k_1 = \theta/(1-\theta)P, \text{ or } \theta = KP/1+KP,$$

Where P is the partial pressure of the gas or the molar concentration of the solution. For every low pressure $\theta \approx KP$, and for high pressure $\theta \approx 1$.

ADSORBENT USED



Fig.1 pistachio nut shell



Fig.2 crushed pistachio Nut shell



Fig.3 pistachio nut shell carbon

The use of pistachio nut shell carbon as an adsorbent of the industrial pollutant is a new trend. The pistachio nut shell carbon has a capability as an adsorbent since it has high carbon content and density low ash content and uniform pore distribution. As an agriculture waste material, the use of pistachio nut shell carbon also becomes a solution for environment. Problems with a low-cost production. Moreover, Iran is a tropical country that provides a large number of pistachio nut shell as a raw material for carbon.

Pistachio nut shell carbon are unique and versatile adsorbent and they are used for the removal of undesirable odour, colour, taste, and other organic and inorganic impurities (generally referred to as adsorbates) from domestic and industrial wastes, for air purification in inhabited places, restaurants, food processing, removal of color from various syrups and pharmaceutical products, in air pollution control from industrial and automobile exhaust and in a variety of gas phase applications. They are also well known for

their applications in medicine for the removal of toxins and bacterial infections in certain alignments.

Adsorption by pistachio nut shell carbon is one of the most frequently used method to remove organic compounds from water, because pistachio nut shell carbon possess perfect adsorption ability for chloro phenols. In this project, the objective is to investigate how the adsorption capacity of pistachio nut shell carbon is influenced by elevated temperature using different concentrations of para-chlorophenol as the adsorbate.

STRUCTURE OF PISTACHIO NUT SHELL CARBON

Adsorption takes place at the surface of pistachio nut shell carbon. The surface characteristics of pistachio nut shell carbon play a crucial role in adsorption from aqueous solutions and catalytic properties of carbon. The structure of pistachio nut shell carbon is classified based on the activities that occur at the surface of the carbon. The structure of pistachio nut shell carbon surface can therefore be viewed in two dimensions namely, physical structure and chemical structure.

PHYSICAL STRUCTURE OF PISTACHIO NUT SHELL CARBON

This refers to how the atoms of pistachio nut shell carbon is linked together and how this arrangement actually give rise to the adsorption ability of pistachio nut shell carbon it also describes the various for sizes available on the surface of pistachio nut shell carbon which is responsible for its wide range of applicability in the sense that the four size of any particular pistachio nut shell carbon determine to a large extent what it is used for. The physical structure of pistachio nut shell carbon is further divided into:

POROUS STRUCTURE

Non-graphitizing carbon (i.e. pistachio nut shell carbon with a random arrangement of microcrystalline, strong cross-linking between neighbouring crystallites and well-developed porous structure) was found to have relatively low density (less than 2 gm/cm^3). The porous structure formed during carbonization process is further developed during activation process.

Activation process is a process through which small, low volume pores which increase the surface area of carbon are created within its structure by either heating carbon at temperature changes between 600 to 1200 degree celsius in the absence of oxygen or by impregnating carbon with certain chemicals such as acids, strong bases or salt followed by heating at low temperatures of about 400 to 700 degree Celsius. This process enlarges the diameter of the pores and improve their volume. The nature of the raw material used for the carbonization determines the structure of the pores generated and the pore size distribution. Activation carbon pores are categorized based on their size and their function. Based on their function, we have,

particles consisting of gaps between carbon plates of about 1-5 molecular diameter in size.

PORES FOR TRANSPORT: these are the largest pores within the particle. They vary from pores greater than 5 molecular diameter to visible cracks. They consist of a variety of different sizes and shapes.

Based on their sizes, 3 groups of pores can be distinguished and they are:

- Micro-pores (<2 nm diameter)
- Meso-pores (2-50 nm diameter)
- Macro-pores (>50 nm diameter)

Micro-pores generally contribute to the bulk part of the internal surface area while meso-pores are generally regarded as highways into the carbon particles and are crucial kinetics. According to Dunin and Zaverina, a micro-porous active carbon is produced when the degree of burn-off is less than 50%, micro-porous active carbon is produced when the extent of burn-off is between 50% and 75%, the product will contain a mixture of all types of pores.

The classification of pores by the Dunin is based on their width which represents the distance between the walls of a slit shaped pore. This classification has now been adopted by the international union for pure and applied chemistry.

Adsorption in micropores whose effective radii is less than 2 nm occurs through volume filling with no capillary condensation taking place. The adsorption energy in micro-pores is much larger compared to other pore types, their volume range between 0.15-0.70 cm³/gm.

PREPARATION OF PISTACHIO NUTSHELL CARBON

In the very first step we collect pistachio nut shell and remove dirt and unwanted substances from it. Then the shell is smashed and crushed and put it in a container or furnace and get it for heating. The heating is done until the pistachio nut shell by product it is the pistachio nut shell processed into carbonation of the latter to produce pistachio nut shell carbon in the form of burned carbon. In the run of burning of pistachio nut shell, the heating temperature should be programmed to increase from the room temperature to the desired carbonization temperature. The overall preparation is by chemical method.

Adsorption process by different mono basic acid (Acetic acid, Propionic acid) dibasic acid (Oxalic acid and Succinic acid)

Materials Used: pistachio nut shell carbon, Dibasic acids (Oxalic acid, Malonic acid, Succinic acid and glutaric acid), NaOH, Phenolphthalein, Stoppered bottle, Burette, Pipette, Funnel, Conical flask.

PROCEDURE:

Prepared aqueous solution of acids into numbered flask as labelled, the total volume of each solution is 50 ml taken in Stoppered bottles. Transfer 10 ml of the solution from each bottle into the conical flask. Add 2-3 drops of Phenolphthalein indicator and titrate against NaOH. Once the end point is reached, read the burette reading. The volume of base V_1 . Calculate the actual concentration of oxalic acid C_1 in the flask number 1 to 5 respectively, and write it down in the table. Using practical balance weigh 5 portions of pistachio nut shell carbon, each portion 1 gram. Put pistachio nut shell carbon into number flask into stoppers and shake them, wait for 20 minutes, the process of adsorption is in progress. Mix the mixtures for several times by

shaking the flask. (The process of adsorption is a function of times it is important to put onion peel into flask at the same time to provide adsorption for the same period in each flask). Filter the mixtures into clean and dry flask to avoid disturbing effect of adsorption of acid into filtering paper, remove away the first portion of filtration approximate of 5ml. Determine the final concentration of acid C , in each of the flask after adsorption from each solution, pipette out 10ml of oxalic acid solution and transfer it to clean and dry conical flask. To this conical flask containing oxalic acid solution at 2 to 3 drops of Phenolphthalein indicator. Now, titrate this solution against NaOH in the burette, note down the burette reading. The volume of base V_2

PROCEDURE TABULAR COLUMN:

Dilution of acid

Bottle No.	Vol. of acid added (0.5N)	Volume of water added in ml	Amount of pistachio nut shell carbon added in gm
1	50	00	1
2	40	10	1
3	30	20	1
4	20	30	1
5	10	40	1

TABULAR COLUMN: Oxalic acid

SINO.	Initial concentration of oxalic acid (C_0)	Vol. of titrant taken in ml	Amt. of pistachio shell carbon added in gm	Burette reading	$C_e = B.R \times 0.1/10$ Eq. conc. of acid in ml/L	$X = C_0 - C_e$ 20 amount adsorbed in ml/L	x/m	$\log(x/m)$	$\log C_e$	$C_e(x/m)$
1	0.5	10	1	10.4	0.104	0.0198	0.0198	-1.7033	-0.9829	0.0020592
2	0.4	10	1	8.6	0.086	0.0157	0.0157	-1.8041	-1.0655	0.0013502
3	0.3	10	1	6.2	0.062	0.0119	0.0119	-1.9244	-1.2076	0.0007378
4	0.2	10	1	4.4	0.044	0.0078	0.0078	-2.1079	-1.3565	0.0003432
5	0.1	10	1	2.2	0.022	0.0039	0.0039	-2.4089	-1.6575	0.0000858

TABULAR COLUMN: Malonic acid

SINO.	Initial concentration of oxalic acid (C_0)	Vol. of titrant taken in ml	Amt. of potassium dichromate added in ml	Burette reading	$C_e = B.R \times 0.1/10$ Eq. conc. of acid in mol/dm ³	$X = C_0 - C_e/20$ amount adsorbed in moles	x/m	$\text{Log}(x/m)$	$\text{Log } C_e$	$C_e(x/m)$
1	0.5	10	1	10.8	0.108	0.0196	0.0196	-1.70274	-0.9665	0.0021168
2	0.4	10	1	8.9	0.089	0.01555	0.01555	-1.80826	-1.0506	0.0013839
3	0.3	10	1	6.7	0.067	0.1165	0.1165	-1.93367	-1.1739	0.0007805
4	0.2	10	1	4.7	0.047	0.00765	0.00765	-2.11633	-1.3279	0.0003595
5	0.1	10	1	2.3	0.023	0.00385	0.00385	-2.41453	-1.6382	0.00008855

TABULAR COLUMN: Succinic acid

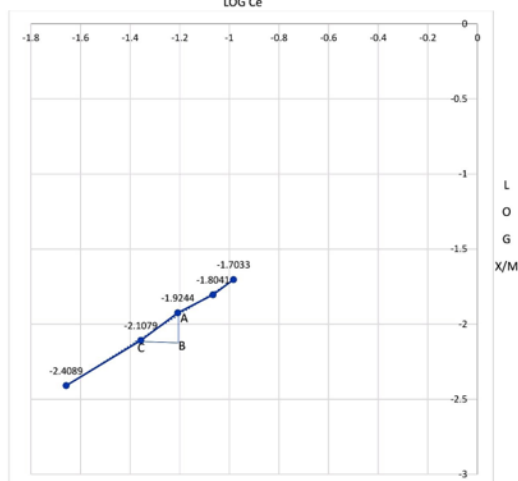
SINO.	Initial concentration of succinic acid (C_0)	Vol. of titrant taken in ml	Amt. of potassium dichromate added in gm	Burette reading	$C_e = B.R \times 0.1/10$ Eq. conc. of acid in mol/dm ³	$X = C_0 - C_e/20$ amount adsorbed in moles	x/m	$\text{Log}(x/m)$	$\text{Log } C_e$	$C_e(x/m)$
1	0.5	10	1	7.8	0.078	0.0211	0.0211	-1.67571	-1.107908	0.001645
2	0.4	10	1	6.4	0.064	0.0168	0.0168	-1.77469	-1.193822	0.001075
3	0.3	10	1	4.4	0.044	0.0128	0.0128	-1.89279	-1.356542	0.000563
4	0.2	10	1	3.4	0.034	0.0083	0.0083	-2.08092	-1.468522	0.000282
5	0.1	10	1	1.7	0.017	0.00415	0.00415	-2.38195	-1.76955	0.00007055

TABULAR COLUMN:

Glutaric acid

SINO.	Initial concentration of oxalic acid (C_0)	Vol. of titrant taken in ml	Amt. of potassium dichromate added in ml	Burette reading	$C_e = B \times 0.1/10$ Eq. conc. of acid in mol/dm ³	$X = C_0 - C_e/20$ amount adsorbed in moles	x/m	Log(x/m)	Log C_e	$C_e(x/m)$
1	0.5	10	1	9.5	0.095	0.02025	0.02025	-1.69357	-1.0227	0.00192375
2	0.4	10	1	7.7	0.077	0.01615	0.01615	-1.79182	-1.11350	0.00124355
3	0.3	10	1	5.5	0.055	0.01225	0.01225	-1.91186	-1.252963	0.00067375
4	0.2	10	1	3.3	0.033	0.00835	0.00835	-2.07831	-1.48148	0.00027555
5	0.1	10	1	1.9	0.019	0.00405	0.00405	-2.39254	-1.72124	0.0000765

EVALUATION OF PISTACHIO NUT SHELL DERIVED ACTIVATED CARBON AS AN ADSORBENT FOR UPTAKE OF DIFFERENT DIBASIC ACIDS

GRAPH: FREUNDLICH ADSORPTION ISOTHERM (OXALIC ACID)
LOG C_e 

Scale= X-axis - 1 unit =0.5cm

Y-axis - 1 unit=0.5cm

$$\text{SLOPE} = \frac{AB}{BC}$$

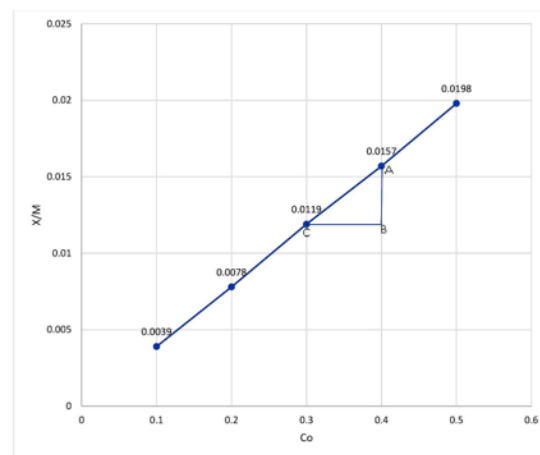
$$= \frac{(-1.9244) - (-2.1079)}{(-1.20) - (-1.35)}$$

$$= \frac{0.1835}{0.15}$$

$$= 1.22$$

EVALUATION OF PISTACHIO NUT SHELL DERIVED ACTIVATED CARBON AS AN ADSORBENT FOR UPTAKE OF DIFFERENT DIBASIC ACIDS

GRAPH : LANGMUIR ADSORPTION ISOTHERM (OXALIC ACID)



Scale= X-axis - 1 unit =0.1cm

Y-axis - 1 unit=0.005cm

$$\text{SLOPE} = \frac{AB}{BC}$$

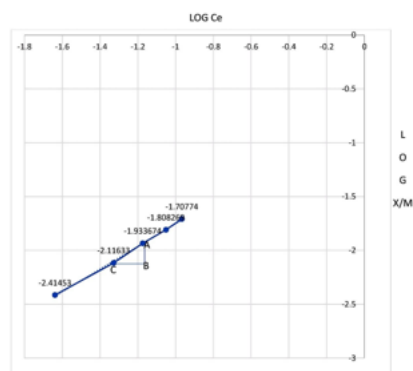
$$= \frac{0.0157 - 0.0119}{0.4 - 0.3}$$

$$= \frac{0.0038}{0.1}$$

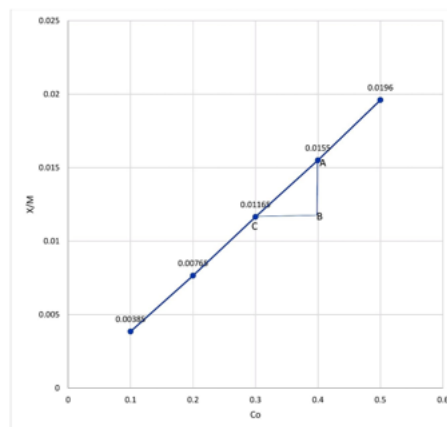
$$= 0.038$$

EVALUATION OF PISTACHIO NUT SHELL DERIVED ACTIVATED CARBON
AS AN ADSORBENT FOR UPTAKE OF DIFFERENT DIBASIC ACIDS

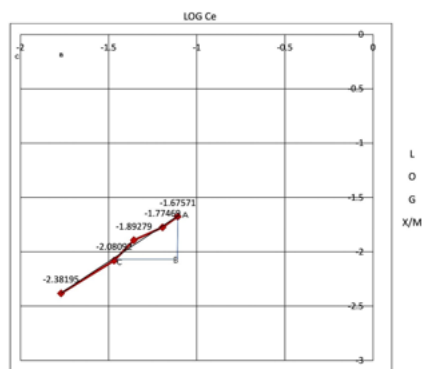
GRAPH: FREUNDLICH ADSORPTION ISOTHERM (MALONIC ACID)

EVALUATION OF PISTACHIO NUT SHELL DERIVED ACTIVATED CARBON
AS AN ADSORBENT FOR UPTAKE OF DIFFERENT DIBASIC ACIDS

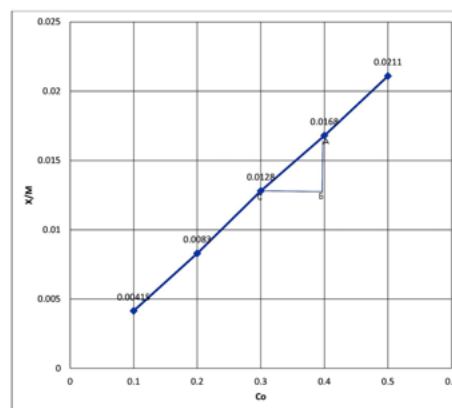
GRAPH : LANGMUIR ADSORPTION ISOTHERM (MALONIC ACID)



GRAPH: FREUNDLICH ADSORPTION ISOTHERM (SUCCINIC ACID)

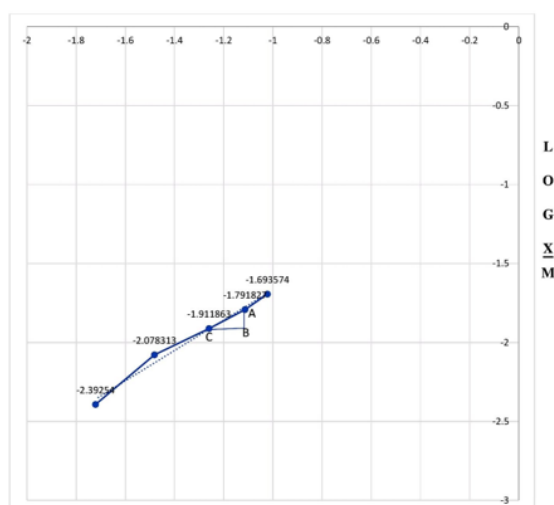


GRAPH : LANGMUIR ADSORPTION ISOTHERM (SUCCINIC ACID)



GRAPH: FREUNDLICH ADSORPTION ISOTHERM (GLUTARIC ACID)

LOG Ce

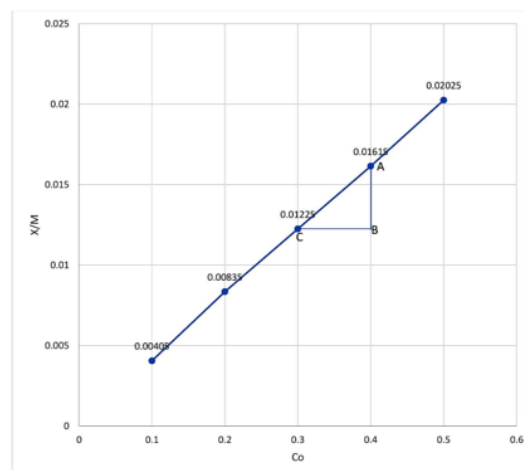


Scale= X-axis – 1 unit =0.5cm

Y-axis- 1 unit=0.5cm

$$\begin{aligned} \text{SLOPE} &= \frac{AB}{BC} \\ &= \frac{(-1.79182) - (-1.91186)}{(-1.11) - (-1.25)} \\ &= \frac{0.12004}{0.14} \\ &= 0.8574 \end{aligned}$$

GRAPH : LANGMUIR ADSORPTION ISOTHERM (GLUTARIC ACID)



Scale= X-axis – 1 unit =0.1cm

Y-axis- 1 unit=0.005cm

$$\begin{aligned} \text{SLOPE} &= \frac{AB}{BC} \\ &= \frac{0.01615 - 0.01225}{0.4 - 0.3} \\ &= \frac{0.0039}{0.1} \\ &= 0.039 \end{aligned}$$

APPLICATIONS OF ADSORPTION

The phenomenon of adsorption finds extensive applications in industry, in laboratory and also in various chemical processes. A few important applications are listed below:

1. Removal of coloring matter:
2. In gas masks:
3. In separating noble gases:
4. In dyeing of cloth:
5. In dehumidizers:
6. Heterogeneous catalysts:
7. In chromatography:
8. In ion exchange resins:
9. In quantitative analysis:
10. In adsorption indicators:
11. In creating high vacuum:
12. In froth floatation process:

CONCLUSION

From the readings obtained it was observed that extent of adsorption of oxalic acid (0.01182), malonic acid (0.01166), succinic acid (0.01263) and glutaric acid (0.01221) reason behind the above conclusion may be the presence of CH_2 group. the extent of adsorption of succinic acid (0.01263) > oxalic acid (0.01182) the reason behind the above conclusion is the presence of 2CH_2 group in succinic acid or absence of 2CH_2 group in oxalic acid.

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